

Name : .....

Roll No. : .....

Invigilator's Signature : .....

**CS / B.TECH(CHE) / SEM-6 / CHE-604 / 2012**  
**2012**  
**NUMERICAL METHODS IN CHEMICAL**  
**ENGINEERING**

Time Allotted : 3 Hours

Full Marks : 70

*The figures in the margin indicate full marks.*

*Candidates are required to give their answers in their own words  
as far as practicable.*

**GROUP – A**

**( Multiple Choice Type Questions )**

1. Choose the correct alternatives for any *ten* of the following :

10 × 1 = 10

i) The Secant method formula for finding the square root of a real number 'R' from the equation  $x^2 - R = 0$  is

a)  $\frac{x_i x_{i-1} + R}{x_i + x_{i-1}}$

b)  $\frac{x_i x_{i-1}}{x_i + x_{i-1}}$

c)  $\frac{1}{2} \left( x_i + \frac{R}{x_i} \right)$

d)  $\frac{2x_i^2 + x_i x_{i-1} - R}{x_i + x_{i-1}}$

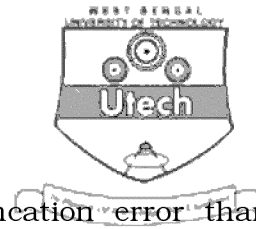
ii) If for a real continuous function  $f(x)$ ,  $f(a) f(b) < 0$  then in the range of  $[a, b]$  for  $f(x) = 0$ , there is (are)

a) one root

b) undeterminable number of roots

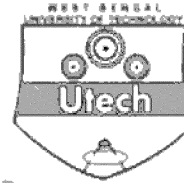
c) no root

d) at least one root.



- iii) Huen's method is
- a) The method having more Truncation error than Euler's method
  - b) 1st order Runge-Kutta Method
  - c) not an iterative method
  - d) 2nd order Runge-Kutta Method
- iv) A heated rectangular slab has one of its sides held at constant heat flux. The other three sides are held at constant temperatures of  $50^\circ$ ,  $25^\circ$  and  $75^\circ$  C. Considering 3 interior nodes in the  $x$  and  $y$  direction each, numerical differencing scheme will generate a
- a)  $9 \times 9$  matrix
  - b)  $12 \times 9$  matrix
  - c)  $9 \times 12$  matrix
  - d)  $12 \times 12$  matrix.
- v) The Explicit scheme for solving the heat conduction equation is both convergent, stable and will not have oscillating solutions if
- a)  $\Delta t \leq \frac{\Delta x^2}{k}$
  - b)  $\Delta t \leq \frac{\Delta x^2}{2k}$
  - c)  $\Delta t \leq \frac{\Delta x^2}{4k}$
  - d)  $\Delta t \leq \frac{2 \Delta x^2}{k}$ .
- vi) Round off the number 86.23852753 up to 5 significant figures
- a) 86.238
  - b) 86.239
  - c) 86.23852
  - d) 86.23853 .



**GROUP - B****( Short Answer Type Questions )**

Answer any *three* of the following.  $3 \times 5 = 15$

2. Find the thermal conductivity ( $k$ ) of propane by using Lagranges interpolation formula at  $1.013 \times 10^4 \text{ kN/m}^2$  and  $99^\circ\text{C}$  from data given in the following table at the same pressure :

Temperature, $T^\circ\text{C}$	68	87	106	140
Thermal conductivity, $k(\text{W/m K})$ at $1.013 \times 10^4 \text{ kN/m}^2$	0.0853	0.0774	0.0699	0.0618

3. Fit the curve  $y = ax'$  by curve fitting method for the following data points (1, 1200), (2, 900), (3, 600), (4, 200), (5, 100), (6, 50).
4. Solve the differential by Euler's method  $dy/dx = x^2y$ , with the initial condition  $y(0) = 1$ . Find  $y(0.3)$ . Compare your result with the analytical solution.
5. Solve the following system of equation with partial pivoting :

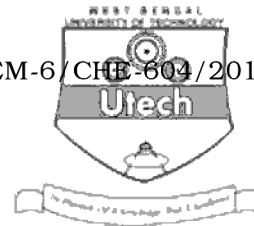
$$2x - 6y - z = -38$$

$$-3x - y + 7z = -34$$

$$-8x - y + 2z = -20$$

6. Evaluate the following integral using Simpson's  $\frac{1}{3}$ rd rule

$$\int_0^4 (1 - e^{-2x}) dx \quad (\text{Taking } n = 0.5).$$

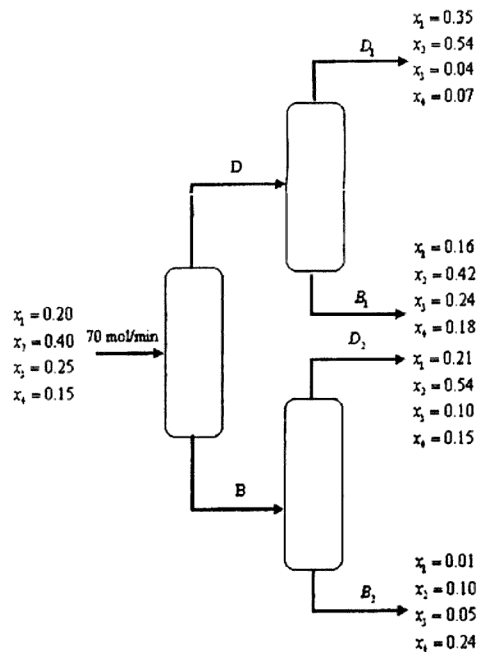


**GROUP – C**

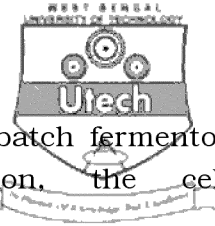
**( Long Answer Type Questions )**

Answer any *three* of the following.  $3 \times 15 = 45$

7. a) Benzene(1), toluene (2), styrene (3) and xylene (4) are to be separated in the sequence of distillation column shown in Fig. Determine molar flow rates of streams  $D_1$ ,  $B_1$ ,  $D_2$  and  $B_2$ . The composition of the feed and the streams  $D_1$ ,  $B_1$ ,  $D_2$  and  $B_2$  is shown in Fig. Also determine the molar flow rates and composition of  $B$  and  $D$ . The molar flow rate of the stream is 70 mol/min.



- b) Find a real root equation  $x^2 - x - 1 = 0$  by Bijection method up to 4 signification figures.  $10 + 5$



8. a) When a microorganism is grown in a batch fermentor under carefully controlled condition, the cell reproduction rate can be modelled as :

$$\frac{dy_1}{dt} = b_1 y_1 \left( 1 - \frac{y_1}{b_2} \right)$$

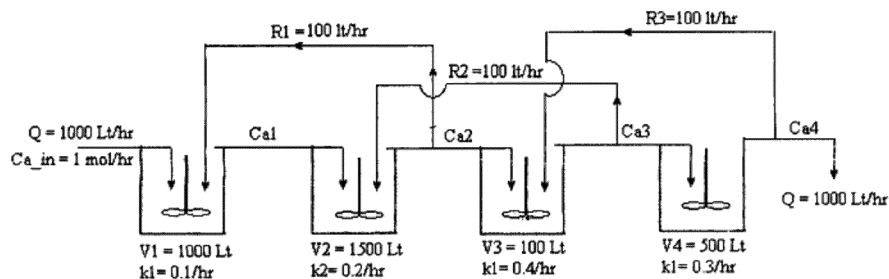
where  $y_1$  is the concentration of cells expressed as percentage dry weight. In addition, the rate of production of the microorganism,  $y_2$  has been found to obey  $\frac{dy_2}{dt} = b_3 y_1 - b_4 y_2$  where  $y_2$  is the units of microorganism per mL. Given that  $b_1 = 0.1$ ,  $b_2 = 4$ ,  $b_3 = 0.02$  and  $b_4 = 0.02$ , evaluate  $y_1$  and  $y_2$  at time = 50 hours if the initial values of  $y_1$  is 0.18 per cent dry weight and  $y_2$  is 0.2 units/ml.

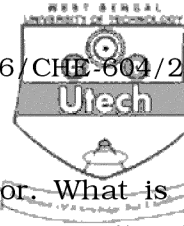
- b) It is desired to solve the following equation :

$f(x) = x^3 - 5x^2 + 7x - 3 = 0$  by Newton-Raphson Method, but it is observed that the good initial guess like  $x^{(0)} = 0$  requires a large number of iteration to find one root  $x = 1$ . Justify the above observation and suggest some modification to reduce the number of iteration.

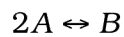
10 + 5

9. a) A set of isothermal CSTR is operated in series with recycle. Find the outlet concentrations from each of CSTR.





- b) Illustrate the concept of truncation error. What is the basis of obtaining the initial guess for any iterative method to be applicable for practical problem ? 10 + 5
10. The catalytic gas phase reaction between components A and B is occurring reversibly in a catalyst layer at a particular point in a monolithic reactor.



The catalytic reaction rate expression for reactant A is given by  $r_A = -k(C_A^2 - C_B / K_C)$

where the rate is in g-mole /cm<sup>3</sup>/s, the rate constant  $k$  has been determined to be  $8 \times 10^4$  in cm<sup>3</sup>/s. g-mole, and the equilibrium constant is known to be  $K_C = 6 \times 10^5$  cm<sup>3</sup>/g-mol. The catalytic layer has a thickness of  $L = 0.2$  cm, and the effective diffusivity of A in B, for this layer is  $D_e = 0.01$  cm<sup>2</sup>/s. The reactant mixture contains only gases A and B, so only binary gas diffusion need be considered. The total concentration of A and B is  $C_T = 4 \times 10^{-5}$  g-mol/cm<sup>3</sup>. Calculation of the effectiveness factor requires consideration of the simultaneous diffusion of both components along with material balance involving the reversible reaction rate expression.

Use an implicit finite difference technique to calculate the effectiveness factor for the given reaction and summarize  $C_A$  and  $N_A$  in a table at 10 equally spaced intervals within the catalytic layer. The reactant concentration at the surface of the layer are known to be  $C_{AS} = 3 \times 10^{-5}$  g-mol/cm<sup>3</sup> and  $C_{BS} = 1 \times 10^{-5}$  g-mole/cm<sup>3</sup>.



11. a) Water is following through a pipe line 6 cm in diameter. The local velocities at various radial positions are given below:

$u$ , cm/s	2.00	1.94	1.78	1.50	1.11	0.61	0.00
$r$ , cm	0	0.5	1.0	1.5	2.0	2.5	3.0

Estimate the average velocity  $\bar{u}$  by Simpson's  $\frac{2}{3}$ -rd rule .

- b) The operation of a constant density plug flow reactor for the production of a substance by an enzymatic is described by the equation :
- $$\frac{V}{F} = - \int_{C_{in}}^{C_{out}} \frac{K}{k_{max}C} + \frac{1}{k_{max}} dC$$
- where  $V$  is volume of the reactor,  $F$  is the flow rate of the reactant,  $C$ .  $C_{in}$  and  $C_{out}$  are the concentrations of reactants entering and leaving the reactor respectively and  $K$  and  $k_{max}$  are constants. For a 500L reactor, with an inlet concentration of  $C_{in}=0.5$  M and inlet flow rate of 40 L/s,  $k_{max} = 5 \times 10^{-3} \text{ s}^{-1}$  and  $K = 0.1$  M, find the concentration of  $C$  at the outlet of the reactor.
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